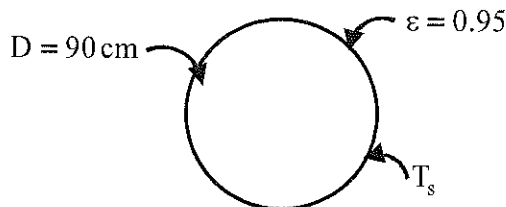


CANKAYA UNIVERSITY
 FACULTY OF ENGINEERING AND ARCHITECTURE
 MECHANICAL ENGINEERING DEPARTMENT

ME 313 Heat Transfer
 Midter Exam I
 FALL 2018

Show all steps of your work to get partial credit

1. The onboard power system of a small deep space probe steadily generates 3 kW energy. The probes' components are enclosed by 90-cm diameter spherical aluminum shell. To minimize the surface temperature of the shell, and therefore the components within it, the shell's outside surface is covered by a very thin layer of special paint with an emissivity of $\epsilon = 0.95$. What is the outside surface temperature of the aluminum shell? What is the heat flux?



outer space is at 0 K

1- steady state

$$\dot{E}_{in} - \dot{E}_{out} + \dot{E}_g = \dot{E}_{st}$$

$$\dot{E}_g = \dot{E}_{out}$$

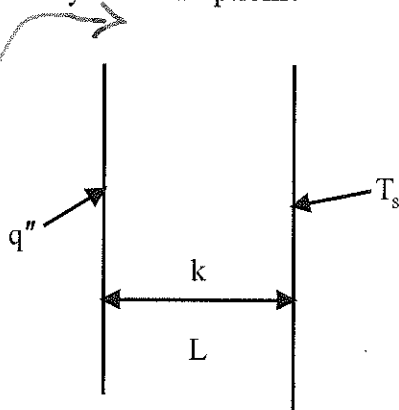
$$= \epsilon \sigma A_s [T_s^4 - T_{sur}^4]$$

$$= \epsilon \sigma A_s T_s^4$$

$$T_s = \left[\frac{\dot{E}_g}{\epsilon \sigma A_s} \right]^{1/4} = \left[\frac{\dot{E}_g}{\epsilon \sigma \pi D^2} \right]^{1/4}$$

$$= \left[\frac{3000 \text{ W}}{(0.95)(0.9)^2 (\pi)(5.669 \times 10^{-8})} \right]^{1/4} \approx 385 \text{ K}$$

2. Consider a plane wall of thickness L and thermal conductivity k . One side of the wall is exposed to a steady heat flux q'' , while the back side is maintained at temperature T_s .
- Obtain the differential equation that governs the temperature distribution in the wall and write the boundary conditions
 - Find the temperature distribution in the wall
 - Find the temperature at $x=0$
- State your assumptions.



$$\rightarrow \frac{d}{dx} \left(A q'' \right) + \frac{d}{dx} \left(A q'' \right) dx$$

$$q'' = -k \frac{dT}{dx}$$

$$\text{So } \frac{d^2 T}{dx^2} = 0$$

$$-k \frac{dT}{dx} (0) = q''$$

$$T(L) = T_s$$

$$T = C_1 x + C_2$$

$$C_1 = -\frac{q''}{k} \quad C_2 = \frac{q'' L}{k} + T_s$$

$$\frac{T(x) - T_s}{\frac{q'' L}{k}} = 1 - (x/L)$$

At $x=0$ $T(0) = \frac{q'' L}{k} + T_s$

Assumption

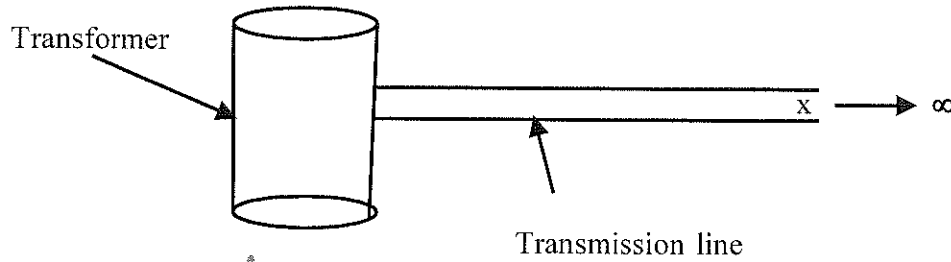
a) steady state

b) one dimensional conduction

c) constant ρ, c, k

d) no energy generation

3) A transformer at a power station experiences a short circuit, resulting in a steady power dissipation of 300 W into a transmission line, which acts as a long fin emanating from the transformer. The transmission line has a diameter of 2 cm and is made of an aluminum alloy ($k=190 \text{ W/m.K}$). The melting temperature of aluminum is 660°C . The air temperature and heat transfer coefficient are 20°C and $\bar{h} = 40 \text{ W/m}^2\cdot\text{K}$ respectively. What is the temperature of the transmission line at its connection point with the transformer? Is the transmission line at risk of experiencing a failure?



- 1- steady state
- One dimensional conduction, $T=T(x)$
- 2- fin is infinitely long
- 3- no radiation
- 4- constant \bar{h}
- 5- constant properties

$$\frac{1 dx}{A} \left(-k \frac{dT}{dx} \right) + \frac{d}{dx} \left(A k \frac{dT}{dx} \right) dx = \bar{h} P dx (T - T_\infty)$$

$$\frac{d^2 T}{dx^2} - m^2 (T - T_\infty) = 0$$

$$x=0 \quad T=T_0$$

$$x=\infty \quad T=T_\infty$$

$$\theta = T - T_\infty$$

$$\frac{d^2 \theta}{dx^2} - m^2 \theta = 0 \quad m = \left(\frac{\bar{h} P}{k A} \right)^{1/2}$$

$$\theta(0) = \theta_0 \quad \theta(\infty) = 0$$

$$\theta(x) = C_1 e^{-mx} + C_2 e^{mx}$$

$$C_1 = 0 \quad C_2 = \theta_0$$

$$\frac{\theta}{\theta_0} = \frac{T(x) - T_{\infty}}{T_0 - T_{\infty}} = e^{-mx}$$

$$A = \frac{\pi D^2}{4} = 3.142 \times 10^{-4} \text{ m}^2$$

$$P = \pi D = 0.0628 \text{ m}$$

$$q = -kA \left(\frac{dT}{dx} \right)_{x=0} = kAm \theta_0 = \theta_0 \sqrt{hPKA}$$

$$T_0 = \frac{q_0}{[hPKA]^{1/2}} + T_{\infty}$$

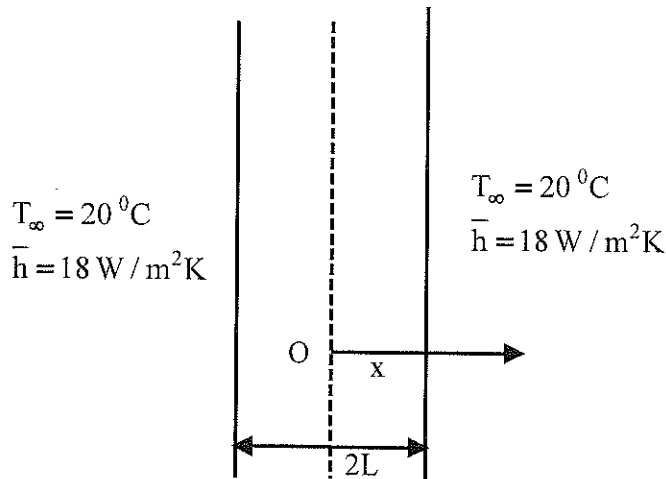
$$T_0 = \frac{390}{[40 \times 0.0628 \times 190 \times 3.142 \times 10^{-4}]^{1/2}} + 20^\circ \text{C}$$

$$= 795^\circ \text{C}$$

$T_0 > T_{\text{melting}}$

Fin will melt, there is a thermal failure.

4.) Upon removal from a 400°C heat treating oven, a large plate of stainless steel ($\rho = 7900 \text{ kg/m}^3$, $c = 480 \text{ J/kg}\cdot\text{K}$, $k = 15 \text{ W/m}\cdot\text{K}$) is allowed to cool in 20°C , where the heat transfer coefficient is $18 \text{ W/m}^2\cdot\text{K}$. If the plate is 25 cm thick, find the center and surface temperature of the plate after cooling for 2 hr .



$$Bi = \frac{\bar{h}L}{k} = \frac{(18 \text{ W/m}^2\text{K})(0.125 \text{ m})}{15 \text{ W/mK}} = 0.15 < 0.1$$

Use Heisler charts

$$\alpha = \frac{k}{\rho c_p} = \frac{15 \text{ W/mK}}{(7900 \text{ kg/m}^3)(480 \text{ J/kg K})} = 3.956 \times 10^{-6} \text{ m}^2/\text{s}$$

$$Fo = \frac{\alpha t}{L^2} = \frac{(3.956 \times 10^{-6} \text{ m}^2/\text{s}) \times 2 \text{ hr} \times \frac{3600 \text{ s}}{\text{hr}}}{(0.125 \text{ m})^2} = 1.8229$$

$$Fo = 1.8229 \quad \left. \begin{array}{l} \\ 1/Bi = 6.66 \end{array} \right\} \frac{\theta_0}{\theta_i} = \frac{T_0 - T_{\infty}}{T_i - T_{\infty}} \approx 0.7891$$

$$T_0 = 0.7891(400 - 20) + 20 = 320^{\circ}\text{C}$$

b) At $x=L$?
 $\frac{x}{L} = 1$ and $1/Bi = 6.66 \Rightarrow \frac{\theta}{\theta_0} = 0.91$

$$\frac{\theta}{\theta_0} = \frac{T - T_\infty}{T_0 - T_\infty} \approx 0.91$$

$$T = T_\infty + 0.91(T_0 - T_\infty)$$

$$= 20 + 0.91(320 - 20)$$

$$= 293^\circ\text{C}$$