

First Name-----

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Last Name-----

Student ID Number-----

Cankaya University
Faculty of Engineering
Mechanical Engineering Department
ME 313 Heat Transfer
Final Exam
Open Book Closed Notes
Fall 2017

Key

1) The spectral emissive power E_λ for a diffusively emitting surface is

$$E_\lambda = \begin{cases} 0 & 0 < \lambda < 3\mu\text{m} \\ 150 \frac{\text{W}}{\text{m}^2 \mu\text{m}} & 3 < \lambda < 12\mu\text{m} \\ 300 \frac{\text{W}}{\text{m}^2 \mu\text{m}} & 12 < \lambda < 25\mu\text{m} \\ 0 & 25 < \lambda < \infty \mu\text{m} \end{cases}$$

Temperature of the surface is 600K.

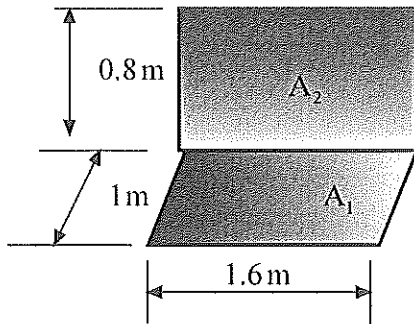
- Calculate the total emissive power of the surface over the entire wavelength.
- Calculate the total hemispherical emissivity of surface
- Calculate the intensity of radiation assuming that intensity is independent of direction.

$$\begin{aligned} \text{a) } E &= \int_0^\infty E_\lambda b d\lambda = \int_0^3 0 d\lambda + \int_3^{12} 150 d\lambda + \int_{12}^{25} 300 d\lambda + \int_{25}^\infty 0 d\lambda \\ &= 0 + 150(12-3) + 300(25-12) + 0 \\ &= 5250 \text{ W/m}^2 \end{aligned}$$

$$\text{b) } \epsilon = \frac{E}{E_b} = \frac{5250}{5.67 \times 10^{-8} (600)^4} = \frac{5250}{7348} = 0.714$$

$$\text{c) } I = \frac{E}{\pi} = \frac{5250}{\pi} = 1671 \text{ W/m}^2 \text{sr}$$

2) Two black rectangular surfaces A_1 and A_2 arranged as shown in the accompanying figure are located in a large room whose walls are black and kept at 300 K. Determine the net heat transfer exchange between these two surfaces when A_1 is kept at 1000 K and A_2 at 500 K. Neglect the radiation from the room.



$$T_1 = 1000 \text{ K}$$

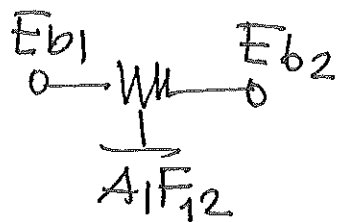
$$T_2 = 500 \text{ K}$$

$$X = 1.6 \text{ m}$$

$$Y = 1 \text{ m}$$

$$Z = 0.8 \text{ m}$$

$$\left. \begin{aligned} \frac{Z}{X} &= \frac{0.8}{1.6} = 0.5 \\ \frac{Y}{X} &= \frac{1}{1.6} = 0.625 \end{aligned} \right\} \text{ Fig 13.6 } F_{12} = 0.2$$



$$q = \frac{Eb_1 - Eb_2}{\frac{1}{A_1 F_{12}}} = A_1 F_{12} (Eb_1 - Eb_2) = A_1 F_{12} \sigma (T_1^4 - T_2^4)$$

$$= (1)(1.6)(0.2)(5.67 \times 10^{-8})(1000^4 - 500^4)$$

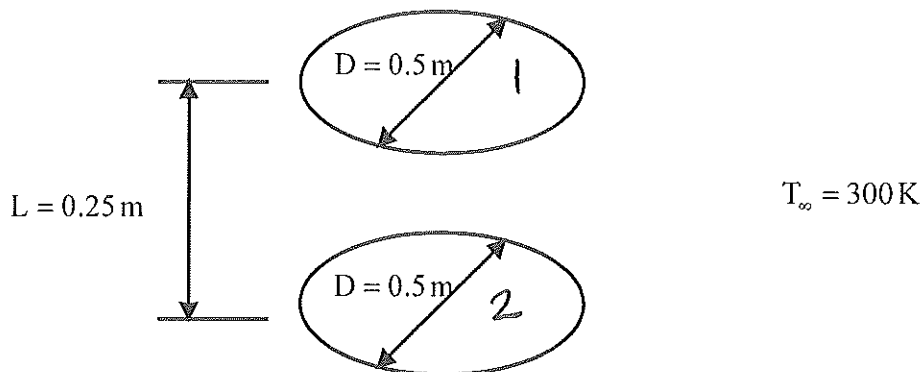
$$= 17000 \text{ W}$$

3) Consider two parallel circular discs of equal diameter $D=0.5$ m separated by $L=0.25$ m

have common control normal as given in the figure. One disk is maintained at $T_1 = 800$ K and has an emissivity $\epsilon_1 = 0.9$. The other is at $T_2 = 500$ K and has an emissivity $\epsilon_2 = 0.7$

. These two parallel discs are exposed through the opening between them into an environment which can be regarded as a black medium at $T_\infty = 300$ K .

- Sketch the radiation network
- Calculate the radiation heat transfer between the two discs
- Calculate the total heat lost into ambient



$$D_1 = 0.5 \text{ m}$$

$$T_1 = 800 \text{ K}$$

$$\epsilon_1 = 0.9$$

$$D_2 = 0.5 \text{ m}$$

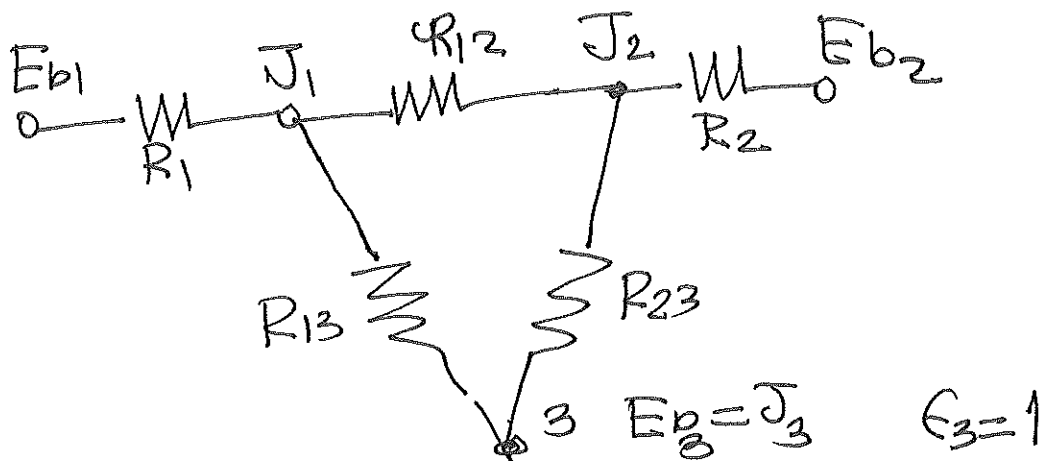
$$T_2 = 500 \text{ K}$$

$$\epsilon_2 = 0.7$$

$$F_{12} = 0.39 \quad A_1 F_{12} = A_2 F_{21} \quad A_1 = A_2 \quad \therefore F_{21} = 0.39$$

$$F_{13} = 1 - 0.39 = 0.61 \quad F_{23} = 1 - 0.39 = 0.61$$

$$A_1 = A_2 = \frac{\pi D^2}{4} = 0.19635$$



$$\epsilon_1 = \frac{1 - \epsilon_1}{A_1 \epsilon_1} = 0.5658$$

$$R_{12} = \frac{1}{A_1 F_{12}} = \frac{1}{\left(\frac{\pi}{16}\right) (6.39)}$$

$$R_2 = \frac{1 - \epsilon_2}{A_2 \epsilon_2} = \frac{1 - 0.7}{\frac{\pi}{16} (0.7)} = 2.182$$

$$= 13.05$$

$$R_3 = \frac{1 - \epsilon_3}{A_3 \epsilon_3} = 0 \quad \text{since } \epsilon_3 = 1$$

$$R_{13} = \frac{1}{A_1 F_{13}} = \frac{1}{\left(\frac{\pi}{16}\right) (0.61)}$$

$$= 8.349$$

$$R_{23} = \frac{1}{A_2 F_{23}} = \frac{1}{\frac{\pi}{16} (0.61)}$$

$$= 8.349$$

$$E_{b1} = \sigma T_1^4 = 23224 \text{ W/m}^2$$

$$E_{b2} = \sigma T_2^4 = 3544 \text{ W/m}^2$$

$$E_{b3} = \sigma T_3^4 = 459.3$$

$$\frac{E_{b1} - J_1}{R_1} + \frac{J_2 - J_1}{R_{12}} + \frac{E_{b3} - J_1}{R_{13}} = 0$$

$$\frac{E_{b2} - J_2}{R_2} + \frac{J_1 - J_2}{R_{12}} + \frac{E_{b3} - J_2}{R_{13}} = 0$$

$$\therefore -1.9434 J_1 + 0.0766 J_2 = -41092$$

$$0.0766 J_1 - 0.6545 J_2 = -16785$$

$$J_1 = 21253 \text{ W/m}^2$$

$$J_2 = 5052 \text{ W/m}^2$$

Net heat transfer

$$q_{12} = \frac{J_1 - J_2}{R_{12}} = \frac{21253 - 5052}{1} = 1241 \text{ W}$$

Heat transfer to environment

$$q = \frac{E_{b3} - J_1}{R_{13}} + \frac{E_{b3} - J_2}{R_{23}} =$$

$$= \frac{459.3 - 21253}{0.1198} + \frac{459.3 - 5052}{0.1198}$$

$$= -3041.3 \text{ W}$$

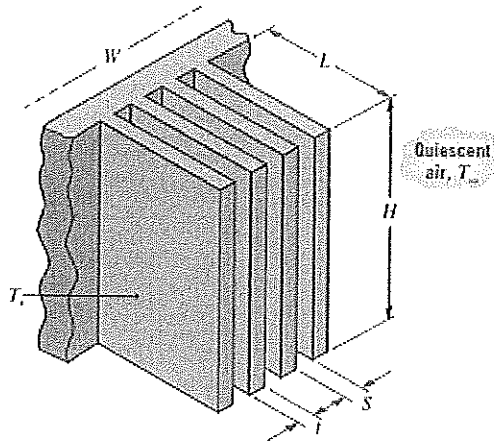
Heat loss from disk 1

$$q_1 = \frac{E_{b1} - J_1}{R_1} = \frac{23244 - 21253}{0.5658} \approx 3519 \text{ W}$$

Heat loss from disk 2

$$q_2 = \frac{E_{b2} - J_2}{R_2} = \frac{3544 - 5052}{2.182} = -691 \text{ W}$$

4) Consider an array of vertical rectangular fins, which is to be used to cool an electronic device mounted in quiescent, atmospheric air at $T_\infty = 27^\circ\text{C}$. Each fin has $L=20\text{ mm}$ and $H=150\text{ mm}$ and operates at an approximately uniform temperature of $T_s = 77^\circ\text{C}$.



There exists an optimum fin spacing $S=34\text{ mm}$. For the optimum value of S and a fin thickness of $t=1.5\text{ mm}$,

- Estimate the number of fins for an array of width $W = 355\text{ mm}$.
- Estimate the total rate of heat transfer from the fins.

Air: At $T_f = 325\text{ K}$ $\nu = 18.41 \times 10^{-6}\text{ m}^2/\text{s}$

$k = 0.0282\text{ W/mK}$ $Pr = 0.703$

From Fig 9.4 of text

$$\eta = \frac{\delta}{H} \left(\frac{Gr_H}{4} \right)^{1/4} \approx 5$$

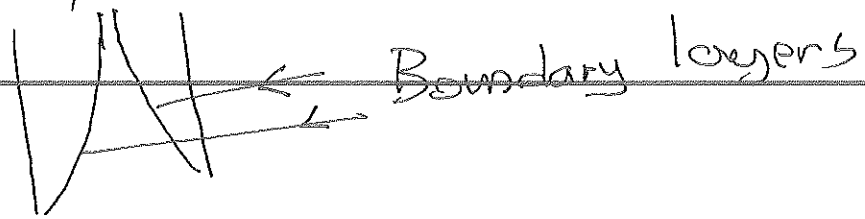
$$\frac{S_{opt}}{t} = \frac{\delta}{x+H}$$

$$Gr_H = \frac{g\beta(T_w - T_\infty)H^3}{\nu^2} = 1.5 \times 10^7$$

$$\delta = \frac{5(0.15\text{ m})}{\left[\frac{1.5 \times 10^7}{4} \right]^{1/4}} \approx 0.017\text{ m} = 17\text{ mm}$$

$S_{opt} \approx 34\text{ mm}$ ← optimum distance between fins. We do not ...

the boundary layers coalesce.



b) # of fins

$$N = \frac{W}{S_{opt} + 1} = \frac{355}{355} \approx 10$$

Heat loss

$$q = 2N \bar{h} (HL) (T_w - T_{\infty})$$

$$\bar{Nu}_H = \bar{Nu}_L = 0.68 + \frac{0.67 Ra_L^{1/4}}{\left[1 + \left(\frac{0.492}{Pr}\right)^{9/16}\right]^{4/9} = 30}$$

$$\bar{h} = \frac{k}{H} \bar{Nu}_H = 5.6 \text{ W/m}^2\text{K}$$

$$q = 16.8 \text{ W}$$